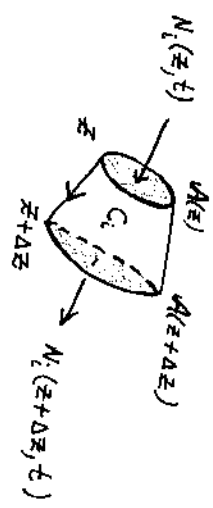


Diffusion Theory { 1-D and quasi 1-D flux in Binary Systems

Typical Element



Geometry	z var.	A(z)	N _i
Linear	z	Constant	N _{i,z}
Cylindrical	r + const	∝ r	N _{i,r}
Spherical	r + const.	∝ r ²	N _{i,r}

Mass Balance on Element, Species i:

$$\frac{\partial}{\partial t} [c_i A \Delta z] = [N_{i,A}]_z - [N_{i,A}]_{z+\Delta z} + [r_i A \Delta z]$$

Accumulation = In. - Out. + Gen.

let $\Delta z \rightarrow 0$

General 1-dim. balances

$$\frac{\partial c_i}{\partial t} = -\frac{1}{A} \frac{\partial}{\partial z} (A N_i) + r_i$$

MT1

i = 1, 2, ...

+ Rate laws

$$\begin{cases} r_i(c_1, c_2, \dots), \text{ and} \\ N_i = B_i + J_i \\ J_i = J_i \left(\frac{dc_1}{dz}, \frac{dc_2}{dz}, \dots \right) \end{cases}$$

Diffusion flux.

+ B.C.'s

2. Fick's laws - Binary Mixtures (or for "dilute" Systems)

$$N_A = B_A + J_A$$

$$B_A = \mathcal{K}_A N \equiv \mathcal{K}_A (N_A + N_B)$$

$$J_A = -D_{AB} C \frac{d\mathcal{K}_A}{dz}$$

or

$$\begin{cases} N_A = \mathcal{K}_A N - D_{AB} C \frac{d\mathcal{K}_A}{dz} \\ N_B = \mathcal{K}_B N - D_{BA} C \frac{d\mathcal{K}_B}{dz}, \dots \end{cases}$$

$$(D_{AB} = D_{BA})$$

2. Inert Systems ($N_2 \equiv 0$)

2.1 Steady-State Diffusion (in Binary Systems)

Mass Balance

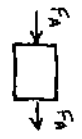
$$\frac{\partial N_A}{\partial t} = -\frac{1}{A} \frac{\partial(A N_A)}{\partial z} + \cancel{N_A} \quad , \text{ etc.}$$

$$\therefore \boxed{A N_A(z) = \text{Constant} = \bar{F}_A, \text{ say}}$$


Geometry

Flux Relation

Linear

$$N_A(z) = \bar{F}_A/A = \text{Const.}$$


Cylindrical

$$N_A(r) = \bar{F}_A / \theta r L = \text{Const.}$$


Spherical

$$N_A(r) = \bar{F}_A / \Omega r^2 = \text{Const.}$$


$\theta =$ Sector of Cylinder

$\Omega =$ Solid angle of Sphere

$L =$ length of cylinder (\perp to figure.)

Similarly $\left\{ \begin{array}{l} A N_A = \bar{F}_A \\ A N_A = \bar{F}_A \end{array} \right.$

Combination with Fick's law gives

$$N_A = N_A N - D_C \frac{dN_A}{dz} = \bar{F}_A / A(z)$$

(where $N = \bar{F}_A / A(z)$ & F, \bar{F}_A are constant)

For constant D_C (e.g. ideal gases, air)

(or for given $D_C(z)$) the above eqn

is a (linear) first-order differential

equation that can be integrated,

boundary condition(s) (There are two

F, \bar{F}_A involved).

§ Example.

Linear Diffusion, $\bar{F}_A/A = \text{Const}$

Integrating gives:

$$\ln(N_A - N_A) = \left(\frac{V}{cD}\right) z + \text{Const}$$

For $N_A = N_{A0}$ at $z = 0$

$N_A = N_{AL}$ at $z = L$

One finds

$$N_A = \frac{C_D}{L \chi_m} (x_{A0} - x_{AL}) = \frac{D}{L \chi_m} (C_{A0} - C_{AL})$$

where (film factor)

$$\chi_m = \log \text{Mean} [(b-1)x_A + 1]$$

$$\stackrel{\text{def}}{=} \frac{[(b-1)x_{A+1}]_o - [(b-1)x_{A+1}]_L}{\ln \left\{ \frac{[(b-1)x_{A+1}]_o}{[(b-1)x_{A+1}]_L} \right\}}$$

and

$$b = -N_B / N_A \quad (\text{Const.})$$

{ other data needed for specification

Other Special Cases:

I.) Stagnant gas B, $N_B \equiv 0 \Rightarrow b = 0$

$$\chi_m = \frac{-(x_{A0} - x_{AL})}{\ln \left(\frac{1-x_{A0}}{1-x_{AL}} \right)}$$

$$\left(N_A = \frac{DC}{L} \ln \left(\frac{x_{oL}}{x_{Bo}} \right) \right)$$

For stagnant film:

$$N = N_A \neq 0$$

Generally: $N = N_A + N_B = (1-b)N_A$

(" Diffusive Convection " - Stefan-N.

II.) " Equimolar Counter-diffusion " ; $N_B = -N_A$

and $N = 0$

$$\chi_m = 1$$

and $N_A = \frac{DC}{L} (x_{A0} - x_{AL}) = \frac{D}{L} (C_{A0} - C_{AL})$

- linear in "driving force" or a gradient.

III.) " Dilute " System (in A) ; x_{A0}, x_{AL} or Negligible Convection ($N \ll N_A$)

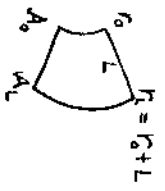
$$\chi_m \approx 1$$

~ Same flux relation as above

Other Geometries (Derive these!)

Cylindrical:

$$F_A = (A N_{A_L}) = (A N_{A_0})$$



$$= \frac{A_M}{\chi_M} \frac{B(C_{A_0} - S_{A_L})}{L}$$

$$A_M = A_{\log\text{mean}} = \frac{A_L - A_0}{\ln(A_L/A_0)} = \frac{2B(r_1 - r_0)}{\ln(r_1/r_0)}$$

Spherical: Same as above, with

$$A_M \equiv A_{\text{geo. mean}} = \sqrt{A_0 A_L} = 2B r_0 r_L$$

Approximate: (e.g. \rightarrow \rightarrow)

Same, with

$$A_M = \left[\frac{1}{L} \int_0^L \frac{dA}{A(x)} \right]^{-1}$$