

# Reference Sheet - Basic Equations

## Property Evaluation

$$v = (1-x)v_f + xv_g, \quad x = \frac{m_{vap}}{m_{liq} + m_{vap}}$$

$$c_v = \left. \frac{\partial u}{\partial T} \right|_v, \quad c_p = \left. \frac{\partial h}{\partial T} \right|_p, \quad h = u + pv$$

$$pv = RT$$

$$Tds = du + pdv$$

$$Tds = dh - vdp$$

$$s_2(T_2, p_2) - s_1(T_1, p_1) = s^\circ(T_2) - s^\circ(T_1) - R \ln \frac{p_2}{p_1}$$

## Compression/Expansion Work

$$W = \int_{V_1}^{V_2} p dV$$

## Closed System - Conservation of Energy

$$\Delta E = \Delta U + \Delta KE + \Delta PE = Q_{in} + W_{in} - Q_{out} - W_{out}$$

$$\frac{dE}{dt} = \dot{Q}_{in} + \dot{W}_{in} - \dot{Q}_{out} - \dot{W}_{out}$$

## Control Volume - Conservation of Mass

$$\frac{dm_{CV}}{dt} = \sum_i \dot{m}_i - \sum_e \dot{m}_e$$

## Mass Flow Rate (1D flow)

$$\dot{m} = \rho AV = \frac{AV}{v}$$

## Control Volume - Conservation of Energy

$$\frac{dE_{CV}}{dt} = \dot{Q}_{CV, in} + \dot{W}_{CV, in} + \sum_i \dot{m}_i \left( h + \frac{V^2}{2} + gz \right)_i - \dot{Q}_{CV, out} - \dot{W}_{CV, out} - \sum_e \dot{m}_e \left( h + \frac{V^2}{2} + gz \right)_e$$

cont.

### Closed System - Entropy Balance

$$S_2 - S_1 = \int_1^2 \left( \frac{\delta Q_{in}}{T} \right)_b - \int_1^2 \left( \frac{\delta Q_{out}}{T} \right)_b + \sigma$$

### Internally Reversible Processes

$$\left( \frac{Q_{net\ in}}{m} \right)_{int\ rev} = \int_1^2 T ds, \quad \left( \frac{W_{net\ out}}{m} \right)_{int\ rev} = \int_1^2 p dv$$

### Control Volume - Entropy Balance

$$\frac{dS_{CV}}{dt} = \sum_j \frac{\dot{Q}_{in,j}}{T_j} - \sum_l \frac{\dot{Q}_{out,l}}{T_l} + \sum_i \dot{m}_i s_i - \sum_e \dot{m}_e s_e + \dot{\sigma}$$

### Isentropic Efficiencies

$$\eta_{turbine} = \frac{(\dot{W}/\dot{m})}{(\dot{W}/\dot{m})_s}, \quad \eta_{compressor} = \frac{(\dot{W}/\dot{m})_s}{(\dot{W}/\dot{m})}, \quad \eta_{pump} = \frac{(\dot{W}/\dot{m})_s}{(\dot{W}/\dot{m})}$$

### Internally Reversible, Steady-state Processes

$$\left( \frac{\dot{Q}_{net\ in}}{\dot{m}} \right)_{int\ rev} = \int_1^2 T ds, \quad \left( \frac{\dot{W}_{net\ out}}{\dot{m}} \right)_{int\ rev} = - \int_1^2 v dp + \left( \frac{V_1^2 - V_2^2}{2} \right) + g(z_1 - z_2)$$

### Cycles: Thermal Efficiency, Coefficient of Performance

$$\eta_{th} = \frac{\dot{W}_{net\ out}}{\dot{Q}_{in}}, \quad \beta_{Ref} = \frac{\dot{Q}_C}{\dot{W}_{in}}, \quad \beta_{HP} = \frac{\dot{Q}_H}{\dot{W}_{in}}$$

### Thermodynamic Temperature Scale

$$\left( \frac{Q_C}{Q_H} \right)_{rev\ cycle} = \frac{T_C}{T_H}$$

### Nonreacting Mixtures

$$mf_i = m_i/m, \quad \sum_{i=1}^j mf_i = 1, \quad y_i = n_i/n, \quad \sum_{i=1}^j y_i = 1$$
$$\bar{u} = \sum_{i=1}^j y_i \bar{u}_i, \quad \bar{h} = \sum_{i=1}^j y_i \bar{h}_i,$$

### Reacting Mixtures

$$\bar{h} = \bar{h}_f^\circ + \Delta \bar{h} = \bar{h}_f^\circ + [\bar{h}(T) - \bar{h}(T_{ref})]$$

$$\frac{\dot{Q}_{CV, net\ in}}{\dot{n}_F} - \frac{\dot{W}_{CV, net\ out}}{\dot{n}_F} = \sum_P n_e \bar{h}_e - \sum_R n_i \bar{h}_i$$